

VALVE SIZING BY COMPUTATION

FORMULA KEY

VALVE SIZING BY COMPUTATION

- C_V = Valve flow coefficient
 D = Nominal pipe size, inches
 d_p = Nominal valve size, inches
 F_L = Pressure recovery factor, Liquid (See valve page)
 F_P = Piping geometry factor, which is a capacity correction factor for a valve with reduced inlet and expanded outlet piping of the same size or a valve with expanded outlet piping only. (For Intimidator, see table on facing page.)

$$F_P = \frac{1}{\sqrt{\frac{\sum k C_V^2}{890d^4} + 1}}$$

- F_R = Valve Reynolds Number factor
 = 1 if $C_V > 0.1$ and viscosity < 1000 cs. (consult factory for other applications)
 G = Specific gravity of liquid at flowing temperature
 K = Specific heat ratio (see table)
 $\frac{C_p}{C_v} = \frac{\text{Specific heat at constant pressure}}{\text{Specific heat at constant volume}}$
 M = Molecular weight (see table)
 P_1 = Initial fluid pressure psia
 = $[p_1 (\text{psig}) + 14.7]$

- P_2 = Reduced fluid pressure psia
 = $[p_2 (\text{psig}) + 14.7]$
 P_C = Critical pressure of liquid (water = 3206 psia)
 P_V = Vapor pressure of liquid at inlet temperature (water @ 60°F = 0.2563 psia)
 ΔP = Comparative fluid pressure factor
 = $P_1 - P_2$
 ΔP_C = Critical pressure drop (psi)
 = $P_1 - .96 P_V + .28 \sqrt{\frac{P_V^3}{P_C}}$
 Q = Flow - SCFM or GPM
 T_1 = Initial absolute temperature of gas
 = $[t_1 (^\circ\text{F}) + 460]$
 W = Flow - lb/hr
 X_T = Pressure recovery factor, Gas (See valve page)
 Z = Compressibility factor (Typically = 1)
 $\sum k$ = Valve/piping friction factor
 $1.5 \left(1 - \frac{d^2}{D^2}\right)^2$

STEAM (MASS)

$$C_V = \frac{W}{19.3 F_P P_1 Y F_R} \sqrt{\frac{T_1 Z}{X M}}$$

GAS (VOLUME)

$$C_V = \frac{Q}{7320 F_P P_1 Y F_R} \sqrt{\frac{T_1 M Z}{X}}$$

SUBCRITICAL FLOW

$$\text{if } X < \frac{X_T K}{1.4}$$

$$X = \frac{\Delta P}{P_1} = \frac{P_1 - P_2}{P_1}$$

$$Y = 1 - \frac{X}{2.14 X_T K}$$

CRITICAL FLOW

$$\text{if } X \geq \frac{X_T K}{1.4}$$

$$X = \frac{X_T K}{1.4}$$

$$Y = .667$$

LIQUID (VOLUME)

SUBCRITICAL FLOW

$$\text{if } \Delta P < \Delta P_C F_L^2$$

$$C_V = \frac{Q}{F_P F_R \sqrt{\frac{\Delta P}{G}}}$$

CRITICAL FLOW

$$\text{if } \Delta P \geq \Delta P_C F_L^2$$

$$C_V = \frac{Q}{F_L F_P F_R \sqrt{\frac{\Delta P_C}{G}}}$$

AVERAGE VALUE OF K & M TABLE

	K	M
Air	1.4	29
Nitrogen	1.404	28
Oxygen	1.401	32
Hydrogen	1.41	2
Carbon Dioxide	1.304	44
Steam	1.31	18.3

INTIMIDATOR PIPING GEOMETRY FACTORS

F_p
for Expanded Outlet Only

d/D	Valve Size	1/2		3/4			1				1-1/2			2		
	Port Size	1/4	5/8	1/4	5/8	7/8	1/4	5/8	7/8	1 1/4	7/8	1 1/4	1 3/4	1 1/4	1 3/4	2 1/4
1		1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0
.9		1.0	1.03	1.0	1.01	1.04	1.0	1.0	1.02	1.06	1.0	1.01	1.04	1.0	1.02	1.05
.8		1.0	1.05	1.0	1.02	1.07	1.0	1.01	1.04	1.09	1.01	1.02	1.06	1.01	1.03	1.07
.7		1.0	1.05	1.0	1.02	1.07	1.0	1.01	1.04	1.1	1.01	1.02	1.06	1.01	1.03	1.08
.6		1.0	1.05	1.0	1.02	1.07	1.0	1.01	1.04	1.09	1.01	1.02	1.06	1.01	1.03	1.07
.5		1.0	1.04	1.0	1.02	1.05	1.0	1.0	1.03	1.07	1.01	1.02	1.05	1.01	1.02	1.06
.4		1.0	1.03	1.0	1.01	1.04	1.0	1.0	1.02	1.05	1.0	1.01	1.03	1.0	1.01	1.04
.3		1.0	1.02	1.0	1.01	1.02	1.0	1.0	1.01	1.03	1.0	1.01	1.02	1.0	1.01	1.02

INTIMIDATOR PIPING
GEOMETRY FACTORS

F_p
for Reduced Inlet & Expanded Outlet of the Same Size

d/D	Valve Size	1/2		3/4			1				1-1/2			2		
	Port Size	1/4	5/8	1/4	5/8	7/8	1/4	5/8	7/8	1 1/4	7/8	1 1/4	1 3/4	1 1/4	1 3/4	2 1/4
1		1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0	1.0
.9		1.0	.995	1.0	.997	.993	1.0	.999	.996	.992	.999	.998	.994	.999	.997	.992
.8		.998	.981	.999	.991	.976	1.0	.997	.987	.971	.997	.992	.978	.997	.989	.974
.7		.997	.963	.999	.983	.953	.999	.993	.974	.945	.994	.984	.958	.993	.978	.95
.6		.995	.945	.998	.974	.929	.999	.989	.96	.917	.991	.976	.936	.99	.967	.925
.5		.993	.926	.998	.965	.906	.999	.985	.947	.891	.988	.967	.915	.986	.955	.90
.4		.991	.91	.997	.956	.886	.999	.981	.935	.868	.985	.96	.897	.983	.944	.88
.3		.99	.897	.997	.95	.87	.999	.979	.925	.85	.982	.953	.882	.98	.936	.862

